

Biogas plant in biorefinery concept

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Second Bioeconomy Course České Budějovice 25.5.2017



WASTE – WHAT TO DO WITH







EUROPEAN BIODEGRADABLE WASTE PRODUCTION 13-10⁹ t_{TS} IN 2015

- agriculture residues, food wastes, biodegradable municipal solid waste, waste biomass from gardens,...
- Typical usage = landfilling, combustion, composting, remain on field
- > DECRASE IN LANDIFILLED WASTE BY 65 % TILL 2020

(European Commission, EU 99/31/ES)

WHAT TO DO WITH?



MOTIVATION FOR BIOREFINERY

THERMOCHEMICAL (GASIFICATION, PYROLYSIS) AND BIOCHEMICAL (ALCOHOLIC FERMENTATION, BIOMETHANE, BIOHYDROGEN,...) TREATMENT OF WASTES WHATO TO PRODUCE, HOW TO TREAT IT, LARGE-SCALE APPLICATION?

Bioenergy **Biomass from farms** Biorefinery Biomaterials Biomass from forest. Chemicals Storage, pretreatment and processing Biofuels **Biomass from** municipal solid wastes

BIOREFINERY = ENVIRONMENTALLY FRIENDLY MULTI TECHNOLOGICAL TREATMENT PARALELLY PRODUCING BIOPRODUCTS, BIOFUELS AND BIENERGY



WASTE – HOW TO USE IT?

> WASTE BIOMASS => ALTERNATIVE ENERGY (*BIOOIL, SYNGAS, BIOMETHAN*,

BIOHYDROGEN, BIOETHANOL) AND BIO-CHEMICALS (SACCHARIDES,

ALCOHOLS, ACIDS, FIBRES, ANTIOXIDANTS, ESSENCIAL PRODUCTS, OILS...)

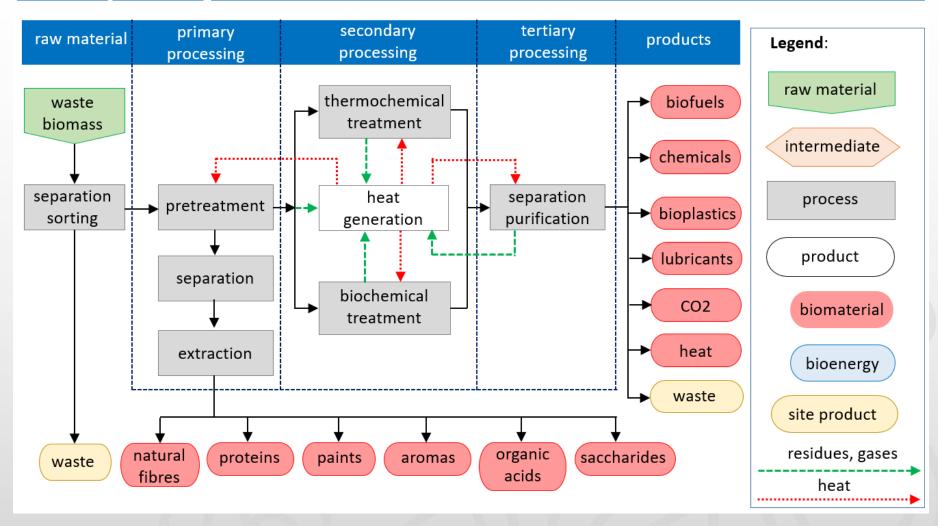


EXAMPLES?

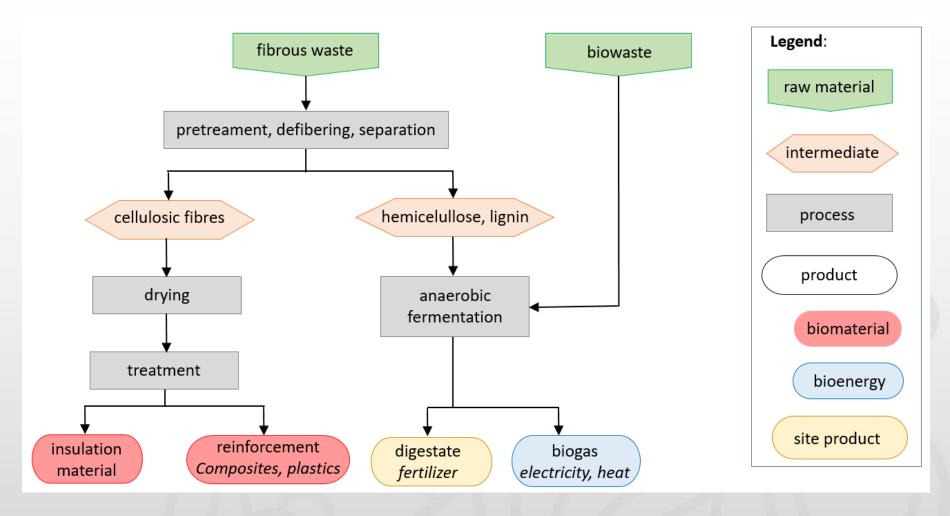


- **PRESSED PEELS OF GRAPES RICH FOR AMYLACOHOLS AFTER FERMENTATION** (*AMYLALCOHOLS* = *SOFTENER FOR PLASTICS*)
- CELLULOSIC FIBRES REINFORCEMENT OF BIOCOMPOSITES
- RICE PEELS RICH FOR SIO2 –> PRODUCTION OF SILICON CARBIDE FIBRES -> CERAMIC REINFORCEMENT OF COMPOSITES
- OIL WEED -> EXTRACTION, BIO-DIESEL PRODUCTION

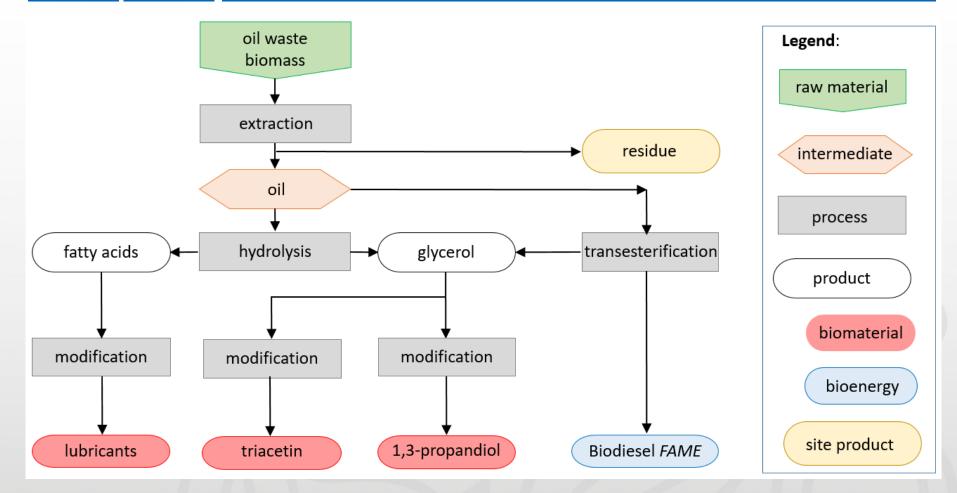




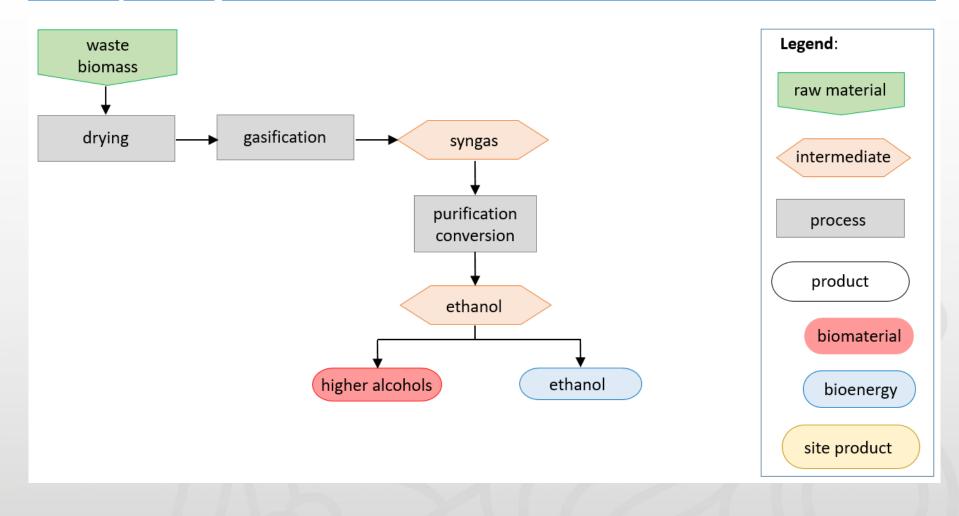






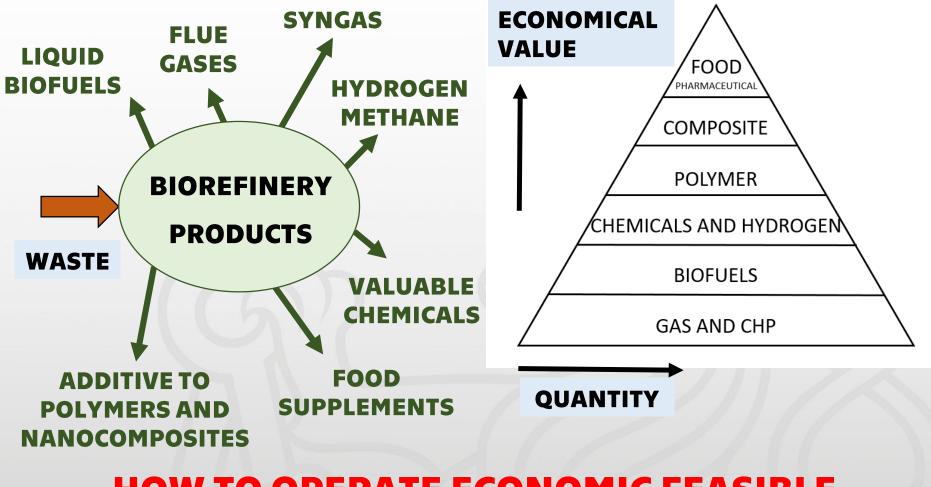






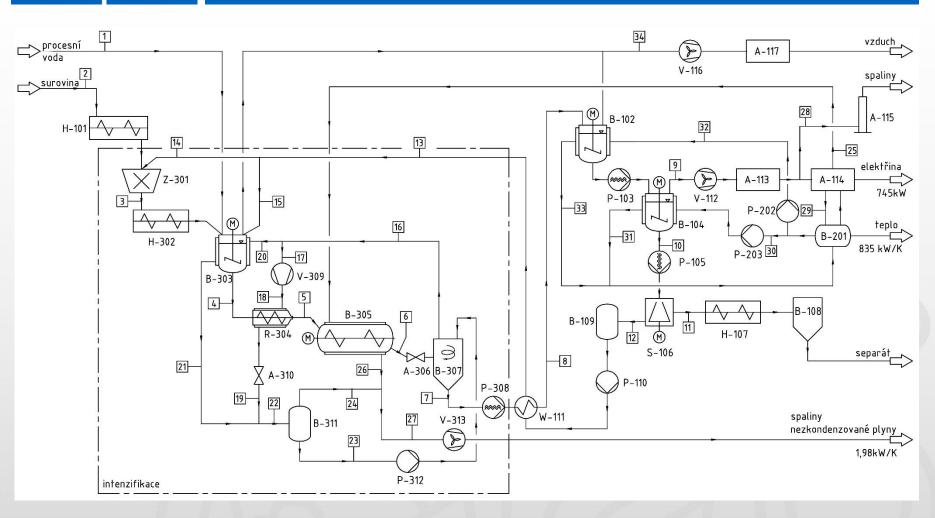


BIOREFINERY'S ECONOMY



HOW TO OPERATE ECONOMIC FEASIBLE TECHNOLOGY WITHOUT SUBSIDIES?

TECHNO-ECONOMICAL FEASIBLE STUDY







BIOREFINERY'S ECONOMY

INVESTMENT COST = ISBL + OSBL + DE + EaE

ISBL – price of apparatuses

OSBL – technology's installation OSBL~ 20-40 % ISBL

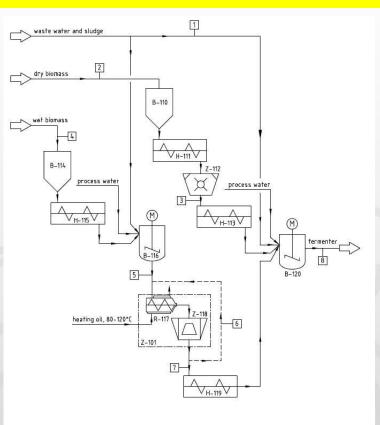
Piping systems, electricity, engineering networks, building, insulation, paints

DE – design and realization

DE ~ 0.1*(ISBL+OSBL)

EaE – financial reserve

EaE ~ 0.1* ISBL Fluctuation in material prices, design and realization work



| | | PROCESS STREAMS | | | | | | | | | |
|---------------|-------|------------------|------------------|-------------------|------------------|----------------------|---------------------|-------------------|-----------------------|--|--|
| | 3 | Biomass input | Biomass input | Milled biomass | Biomass input | Biomass extrusion | Circulation loop | Milled biomass | Biomass to process | | |
| | | 1 | 2 | 3 | 4 | 5 | 6 | 7 | 8 | | |
| moisture | (%hm) | - | 4-20 | 4-20 | >20 | >30 | - | - 19 | 88-92 | | |
| dry matter | (%hm) | | 80-96 | 80-96 | <80 | <70 | 120 | 29 | 8-12 | | |
| particle size | (mm) | 142 | 320 | 1-2 | 127 | 22 | >10 | < 10 | <10 | | |
| temperature | (°C) | 8 <u>-</u> 285 | 222 | 2 | 32203 | <u> </u> | 32 | 50-80 | 30-40 | | |



BIOREFINERY'S PRODUCT COST

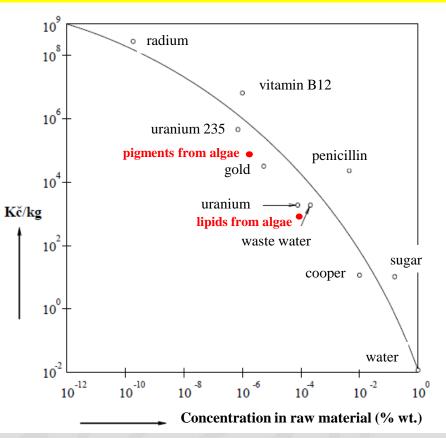
TOTAL PRODUCT COST = OP + GEN

OP- OPERATIONAL COST

consumables,
 operating,
 supervision,
 energy, service
 and maintenance,
 insurance, rates,
 rents and taxes...

GEN- GENERAL COST

Wages, advertising, transport,...



SIMPLE PAYBACK TIME = INV/CSF

INV=INVESTMENT COST; CSF=ANNUAL CASH FLOW



BIOREFINERY'S COST

DEMAND TO TECHNOLOGY

- HIGH CONVERSION EFFICIENCY
- EASY PROCESS, NO OR SIMPLE PRETREATMENT
- NO DEGRADATION OF PRODUCTS
- MINIMUM WASTE GENERATION
- MINIMUM ENERGY DEMAND
- HEAT RECOVERY SYSTEM
- MINIMUM USAGE OF CHEMICALS



BIOREFINERY'S COST

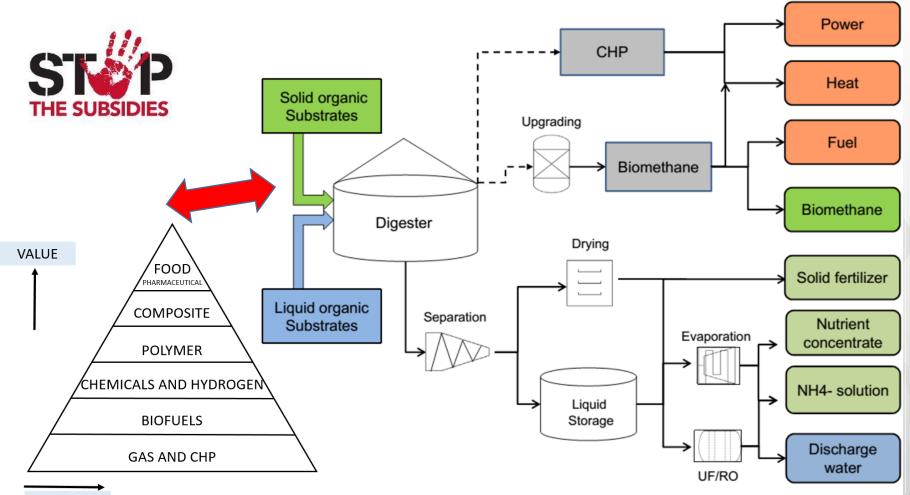
DEMAND TO APPARATUSSES

- EASY CONTROL, SERVICE AND MAINTENANCE
- CORROSION RESISTANCE
- MINIMUM OF EXPENSIVE MATERIALS AND SPECIAL
 PARTS
- COMPROMISE WORKING VOLUME TO PRICE OF EQUIPMENT
- LOW FINANCIAL DEMAND IN INVESTMENT AND
 OPERATION



CONVENTIONAL BIOGAS PLANT

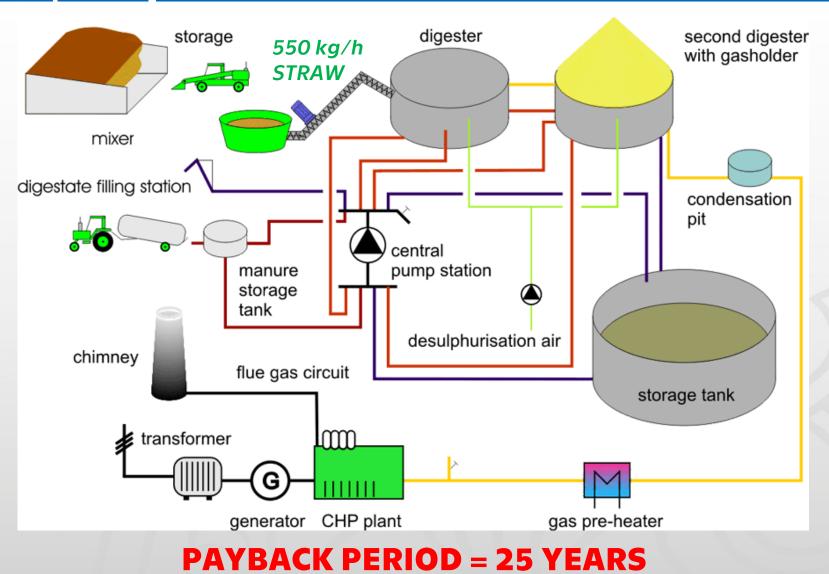
IS THERE POSSIBILITY TO REACH PROFIT WITHOUT SUBSIDIES?



QUANTITY

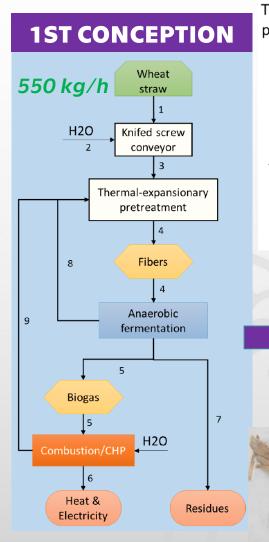


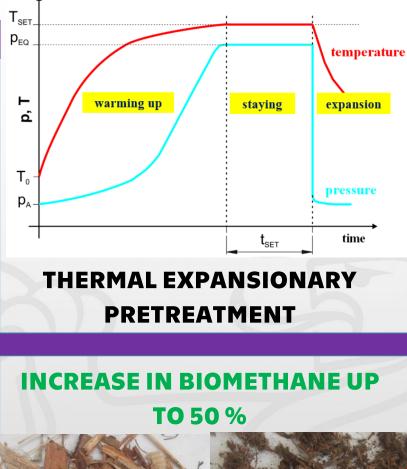
CONVENTIONAL BIOGAS PLANT





UPGRADED BIOGAS PLANT





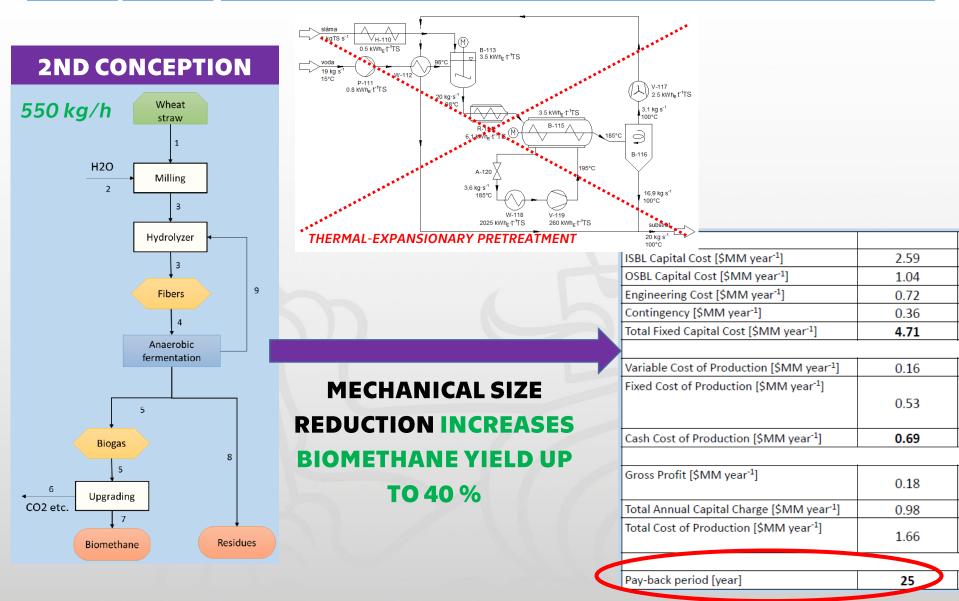
| | ISBL Capital Cost [\$MM year ⁻¹] | 3.8 <mark>1</mark> 6 |
|---|---|----------------------|
| | OSBL Capital Cost [\$MM year ⁻¹] | 1.562 |
| | Engineering Cost [\$MM year ⁻¹] | 1.068 |
| | Contingency [\$MM year ⁻¹] | 0.534 |
| | Total Fixed Capital Cost [\$MM year ⁻¹] | 6.945 |
| | | |
| | Variable Cost of Production [\$MM year ⁻¹] | 0.10 |
| | Fixed Cost of Production [\$MM year ⁻¹] | 0.70 |
| | Cash Cost of Production [\$MM year ⁻¹] | 0.80 |
| | | |
| Y | Gross Profit [\$MM year ⁻¹] | 0.20 |
| | Total Annual Capital Charge | 1.44 |
| | [\$MM year ⁻¹] | |
| | Total Cost of Production [\$MM year ⁻¹] | 2.24 |
| 1 | | |

30

Pay-back period [year]



UPGRADED BIOGAS PLANT

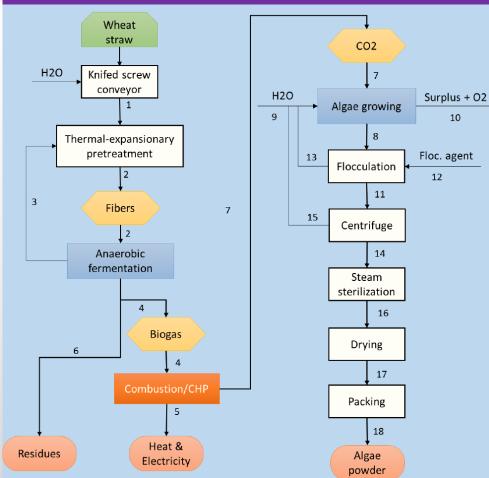




BIOGAS PLANT AS BIOREFINERY

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3TH CONCEPTION



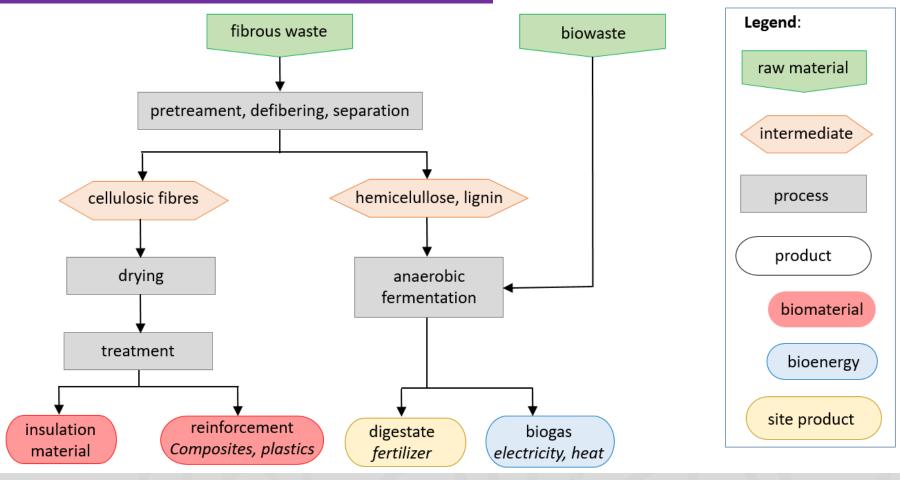
EMISSION GASES AND WASTE HEAT FOR ALGAE PRODUCTION

| | • |
|--|----------|
| | |
| ISBL Capital Cost [\$MM year ⁻¹] | 11.142 |
| OSBL Capital Cost [\$MM year ⁻¹] | 4.457 |
| Engineering Cost [\$MM year ⁻¹] | 4.145 |
| Contingency [\$MM year ⁻¹] | 3.611 |
| Total Fixed Capital Cost [\$MM year-1] | 23.356 |
| | |
| Variable Cost of Production [\$MM year-1] | 4.58 |
| Fixed Cost of Production [\$MM year ⁻¹] | 1.69 |
| Cash Cost of Production [\$MM year ⁻¹] | 6.27 |
| Gross Profit [\$MM year-1] | 0.19 |
| Total Annual Capital Charge [\$MM year ⁻¹] | 4.84 |
| Fotal Cost of Production [\$MM year ⁻¹] | 11.11 |
| | |
| Pay-back period [year] | 59 |



BIOGAS PLANT AS BIOREFINERY

4TH CONCEPTION



PAYBACK PERIOD = 4 YEARS



> THOUSANDS OF STUDIES HOW TO TREAT WASTES

APPLICABILITY IN INDUSTRIAL SCALE?

INDUSTRIAL BIOREFINERY

TECHNO-ECONOMICAL STUDIES ARE URGENT + SCALE UP RULES DEFINITIONS FOR APPARATUSES

